

UDO HÖLKER
KREISLER 1101-KGB

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~~26.~~ A bioreactor for fermenting solid substrates, comprising a fermentation vessel (2), a charging means for bioreactive substances, and a nozzle arrangement within said fermentation vessel (2) for aeration and thorough mixing of the substrates, wherein the at least one nozzle arrangement (10, 20) has a multitude of pipes (14, 24) extending in parallel into the reaction space (49) of the fermentation vessel (2) and provided with nozzles (16, 28), wherein a first, vertically extending nozzle arrangement (10) can be extended into and retracted from the reaction space (49) of the fermentation vessel (2), characterized by a second, horizontal nozzle arrangement with at least one pipe having nozzle orifices and extending horizontally through the reaction space.

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~~27.~~ The bioreactor according to claim ²⁷~~26~~, wherein a second, horizontal nozzle arrangement (20) is provided which consists of at least two interconnected pipes (24) extending horizontally and in parallel through the reaction space (49), each having a plurality of nozzle orifices (28).

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~~28.~~ The bioreactor according to claim ²⁷~~26~~, wherein said horizontal nozzle arrangement (20) can be rotated around a horizontal rotation axis.

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~~29.~~ The bioreactor according to claim ²⁷~~26~~, wherein said fermentation vessel (2) has a bottom section (32) with a tapering cross-section.

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~~30.~~ The bioreactor according to claim ³⁰~~29~~, wherein said conically designed bottom section (32) leads into a draining channel (36) which is inclined from horizontal and has a draining valve (40) at the lowest position thereof.

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~~31.~~ The bioreactor according to claim ²⁷~~26~~, wherein said at least one nozzle arrangement (10, 20) receives compressed gas (48) from a pressure vessel (44, 46).

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~~32.~~ The bioreactor according to claim ³²~~31~~, wherein said pressure vessel (44, 46) contains a bioreactive liquid substance (50) in addition to said compressed gas (48).

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~~33.~~ The bioreactor according to claim ³³~~32~~, wherein said at least one nozzle arrangement (10, 20) alternatively receives compressed air (48) or said liquid bioreactive substance (50) from said pressure vessel (44, 46).

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34. The bioreactor according to claim ²⁷26, wherein said at least one nozzle arrangement (10, 20) can be pressurized with pulsing compressed air (48).

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35. The bioreactor according to claim ²⁷26, wherein said second nozzle arrangement (20) is provided within said fermentation vessel (2) in a height-adjustable manner.

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36. The bioreactor according to claim ³³32, wherein a multitude of pressure vessels (52, 54, 56, 58, 60) pressurized with compressed air (48) and connected to a mixing vessel (46) are provided which contain different liquid bioreactive substances.

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37. The bioreactor according to claim ³⁷36, wherein said mixing vessel (46) has a pressure compensating means (47).

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38. The bioreactor according to claim ³⁷36, wherein said pressure vessels (52, 54, 56, 58, 60) are exchangeable and can be separately autoclaved.

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39. The bioreactor according to claim ³¹38, wherein said draining channel (36) is covered by a wire mesh (38).

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40. The bioreactor according to claim ²⁷26, wherein a pressure lid (8) of said fermentation vessel (2) accommodates said first nozzle arrangement (10) whose pipes (24) extend vertically from the pressure lid (8) into the reaction space (49).

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41. The bioreactor according to claim ⁴¹40, wherein said vertical pipes (14) of said first nozzle arrangement (10) are provided in said pressure lid (8) to be exchangeable.

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42. The bioreactor according to claim ²⁷26, wherein said fermentation vessel (2) is connected through a feed line (74) with a measuring chamber (72), which is again connected through a recirculating line (84) with said fermentation vessel (2), and that said measuring chamber (72) can be pressurized for recirculating measured media.

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43. The bioreactor according to claim ²⁷26, wherein a device for heat exchange is provided, especially comprising a device

- (i) in which said fermentation vessel (2) has a double wall and the thus formed cavity (51a) can be flowed through with temperature-controlled heat exchange fluids through a

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connecting pipe (51b) and discharge pipe (51c); and/or

(ii) which is a horizontal pipe system (20) within said fermentation vessel (2) which can be flowed through with a temperature-controlled heat exchange fluid.

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44. A method for the aerobic fermentation of solid substrates, wherein a reaction medium containing such solid substrates is thoroughly mixed by compressed gas (48) supplied to the reaction medium from above.

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45. The method according to claim ⁴⁵44, wherein said thorough mixing is effected by a continuous stream of compressed gas or by compressed gas pulses.

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46. The method according to claim 44, wherein said solid substances are selected from coal, wood and loaded soils.

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47. The method according to claim ⁴⁷46, wherein said solid substance is coal, especially brown coal (lignite).

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48. The method according to claim ⁴⁸47, wherein a microorganism suitable for fermentation, nutrients and/or buffers are further added to the reaction mixture.

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49. The method according to claim ⁴⁹47, wherein said brown coal or the reaction medium containing said brown coal is tyndallized together with the bioreactor prior to fermentation or prior to the addition of said microorganism.

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50. The method according to claim ⁴⁸47, wherein:

- (i) said brown coal has a particle size of from 1 to 10 mm;
- (ii) said microorganism is selected from molds, yeasts and white rot fungi, especially *Trichoderma atroviride*;
- (iii) the pH of the reaction medium is from 5.5 to 6.0 at the beginning of the reaction;
- (iv) the pH is maintained at from 6.5 to 7.2 during the solubilization phase;
- (v) the fermentation is performed at a temperature of from 25 °C to 30 °C; and/or
- (vi) from 1 to 25 l of compressed air per liter of fermentation broth per day is passed